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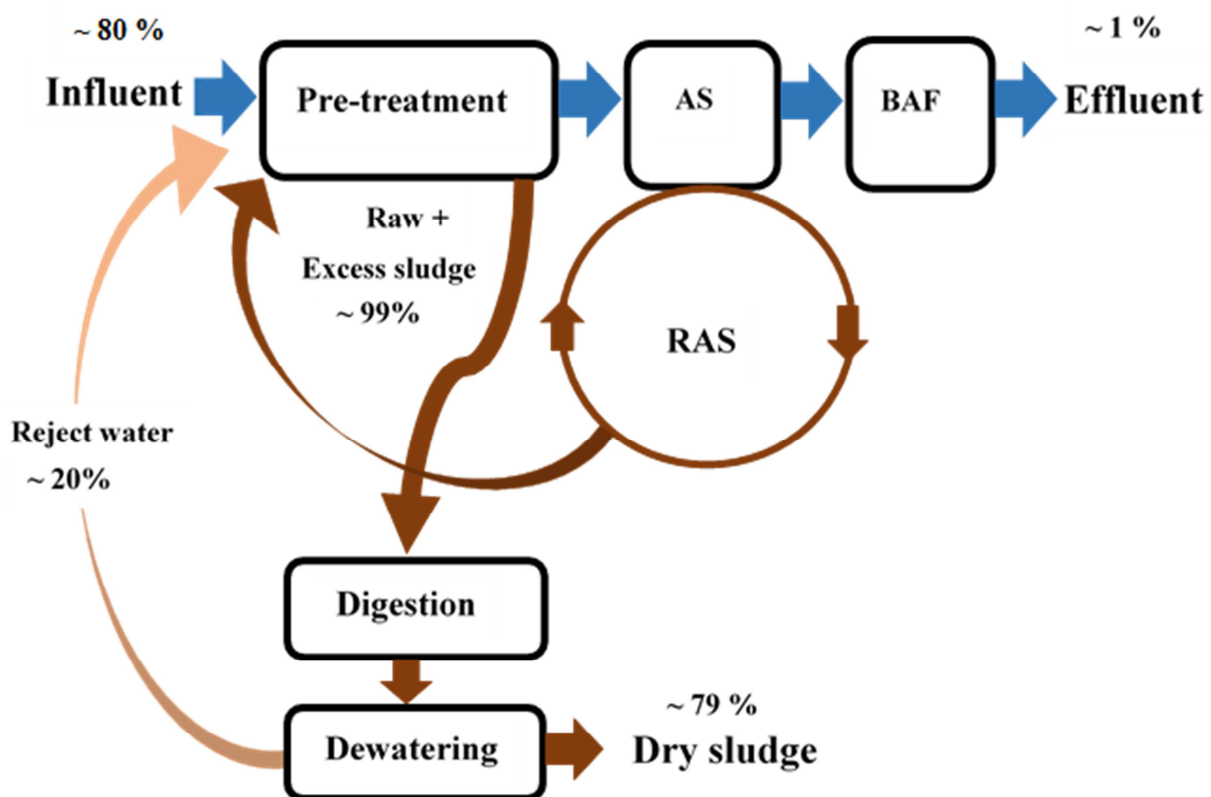
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Micro litter balance for WWTP

1 **How well is microlitter purified from wastewater? – A detailed study on the**
2 **stepwise removal of microlitter in a tertiary level wastewater treatment plant**

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8

9 **Abstract**

10 Wastewater treatment plants (WWTPs) can offer a solution to reduce the point source input of
11 microlitter and microplastics into the environment. To evaluate the contributing processes for
12 microlitter removal, the removal of microlitter from wastewater during different treatment steps of
13 mechanical, chemical and biological treatment (activated sludge) and biologically active filter
14 (BAF) in a large (population equivalent 800 000) advanced WWTP was examined. Most of the
15 microlitter was removed already during the pre-treatment and activated sludge treatment further
16 decreased the microlitter concentration. The overall retention capacity of studied WWTP was over
17 99% and was achieved after secondary treatment. However, despite of the high removal
18 performance, even an advanced WWTP may constitute a considerable source of microlitter and
19 microplastics into the aquatic environment given the large volumes of effluent discharged
20 constantly. The microlitter content of excess sludge, dried sludge and reject water were also
21 examined. According to the balance analyses, approximately 20% of the microlitter removed from
22 the process is recycled back with the reject water, whereas 80% of the microlitter is contained in the
23 dried sludge. The study also looked at easy microlitter sampling protocol with automated composite
24 samplers for possible future monitoring purposes.

25 **Key words:** WWTP, microlitter, microplastics, wastewater, sludge, reject water, microlitter budget

26 1. Introduction

27 Litter has become a serious problem in aquatic environments worldwide. Litter includes both
28 organic and inorganic materials like glass, metals, rubber, wood, paper, textiles and, for the most,
29 plastics (OSPAR 2014). Microlitter comprises litter particles smaller than 5 millimetres. Microlitter,
30 and particularly its plastic subtype, microplastics, has received considerable attention over the past
31 decade (Thompson *et al.* 2004, Barnes *et al.* 2009, Ladewig *et al.* 2015). Microplastics are of
32 concern because of their durability and potential to be transferred within food webs (Cole *et al.*
33 2013, Setälä *et al.* 2014). Microplastics may cause mechanical stress when ingested, but also expose
34 marine organisms to various hazardous substances, such as plasticizers (Fries *et al.* 2013), toxic
35 metals (Rochman *et al.* 2014) and persistent organic pollutants (POPs) (Rios *et al.* 2010, Chua *et al.*
36 2014). These micropollutants are either added to the plastics during production or adsorbed from
37 the surrounding water (Teuten *et al.* 2009). In aquatic environments, microplastics can also function
38 as artificial “microbial reefs” and transport non-indigenous and possibly harmful species (Zettler *et*
39 *al.* 2013). In addition to microplastics, also non-synthetic textile fibers has been proposed to have
40 potential to transport chemical pollutants throughout the aquatic environment (Ladewig *et al.* 2015).
41 Microlitter consists of primary and secondary particles. Primary particles are intentionally
42 microscopic in, e.g. microbeads in peeling lotions and textile fibers, while secondary microlitter is
43 fragmented from larger particles (Barnes *et al.* 2009). Both aquatic and land-based sources have
44 been identified contribute to the amount of litter in marine environments (Law *et al.* 2010). Land
45 base sources include public littering, poorly managed landfills, riverine transport, stormwater and
46 untreated municipal sewage.

47 Recently, wastewater treatment plants (WWTPs) have been suggested to act as one of the land base
48 sources or entrance routes for microlitter to the aquatic environment (Magnusson & Norén 2014,
49 Talvitie *et al.* 2015, Murphy *et al.* 2016). First studies have shown that microlitter can be efficiently
50 (> 98 %) removed from the wastewater during the wastewater treatment (Magnusson & Norén

51 2014, Carr *et al.* 2016, Murphy *et al.* 2016). However, treated effluents still contain microlitter
52 particles like plastic microbeads from toothpaste and textile fibers (Browne *et al.* 2011, Talvitie *et*
53 *al.* 2015, Carr *et al.* 2016).

54 As vast volumes of effluent waters are discharged continuously into aquatic environments globally
55 and the amounts are expected to grow due the population growth and urbanization (UN Water
56 2015), the role of WWTPs as an entrance route of microlitter to aquatic environments may be
57 significant. At the same time, WWTPs can offer solutions to reduce the input of microlitter into the
58 environment. Despite of this potential, very little attention has yet been drawn to the actual removal
59 of microlitter during different type of wastewater treatment processes. Here we report detailed data
60 on the removal of microlitter during different treatment steps in a large (population equivalent
61 800 000) advanced WWTP. The balance of microlitter in WWTP were estimated to further evaluate
62 the removal and distribution of microlitter during the treatment processes. Also, the effect of
63 microlitter size and shape on their removal in different treatment steps were determined. The further
64 objective of this study was to establish an easy-to-use protocol for monitoring of WWTPs. In the
65 end, we report the evaluation of microlitter and microplastic load discharged into the marine
66 environment with effluents.

67

68 **2. Materials and Methods**

69 **2.1 Description of the selected WWTP**

70 Selected WWTP (Viikinmäki, Helsinki Region Environmental Services Authority, HSY) is the
71 largest wastewater treatment plant in Finland and the Nordic Countries, treating the wastewaters of
72 ca. 800,000 inhabitants in the Helsinki metropolitan area. An average of 270 000 cubic meters of
73 treated wastewaters are discharged from the WWTP into a Gulf of Finland, Baltic Sea every day.
74 The treatment process in Viikinmäki WWTP is based on activated sludge method and has multiple
75 treatment steps based on pre-, chemical- and biological treatment. The nitrogen removal has been

76 enhanced with a tertiary denitrifying biological filter. In 2015, 95% of organic material (BOD₇),
77 98% of suspended solids (SS), 95% of total phosphorus (P-tot) and 90% of total nitrogen (N-tot)
78 were removed during the treatment process of the selected WWTP.

79 Pre-treatment includes coarse screening (10 mm), grit removal, chemical treatment and primary
80 sedimentation. In order to remove phosphorus, ferrous sulphate is dosed in the sand removal prior
81 to secondary clarifier. In biological treatment biodegradable matter and nitrogen are removed from
82 the wastewater with activated sludge method. Activated sludge process includes aeration tanks and
83 secondary clarifiers. Hydraulic retention time in the process is approximately 25 hours and sludge
84 retention time varies between 6 – 12 days. Most of the activated sludge is recycled from secondary
85 clarifiers into the aeration tanks as return activated sludge but part of it is also continuously
86 removed from the process. This excess sludge is returned to primary sedimentation and sent to
87 sludge treatment together with raw sludge. The nitrogen removal is further improved in tertiary
88 treatment process with biologically active filter (BAF). During the BAF process, wastewater flows
89 through tightly packed polystyrene beads. The beads provide a surface for micro-organisms to
90 attach and grow. While growing, they consume organic material as well as phosphorus and convert
91 nitrates to nitrogen gas.

92 Viikinmäki WWTP has also a solids handling treatment. Organic matter in the sludge is
93 anaerobically digested to produce biogas, i.e. methane and consecutively used for the plant's own
94 energy consumption. After the digestion, sludge is dewatered with centrifuges. For dewatering, the
95 sludge is conditioned with flocculation chemical polyacrylamide (PAM). PAM induces a release of
96 the water during dewatering by enhancing the aggregation of sludge particles into larger particle
97 groups called flocs. Dewatering generates reject water, which is conducted via a settling tank into
98 the beginning of the wastewater treatment process. The dried sludge is processed further in
99 composting fields and used in green construction. The plant produces annually around 60,000
100 tonnes of dried sludge which has a dry solids (TS) content of 29 %.

101 **2.2 Sampling methods**

102 The samples were collected from the plant influent, after pre-treatment, after the activated sludge
 103 (AS) process, plant effluent, excess sludge, reject water and dried sludge (SD fig. S1). Sampling
 104 was carried out during a seven-day period 14.9 – 20.9.2015 with three different sampling methods;
 105 grab sampling (here meaning one sampling occasion at a certain time), 24-hour composite sampling
 106 and 24- hour sequential sampling (Table 1).

107 Table 1. Sampling methods (grab sampling, 24h composite sampling, 24h sequential sampling),
 108 sampling locations (wastewater, sludge) and sampling days.

	Monday 14.9.2015	Tuesday 15.9.2015	Wednesday 16.9.2015	Thursday 17.9.2015	Friday 18.9.2015	Saturday 19.9.2015	Sunday 20.9.2015
Grab sampling (wastewater)	X		X			X	
Grab sampling (sludge)			X				
Grab sampling (reject water)			X				
24h composite sampling (wastewater)		X		X			X
24h sequential sampling (wastewater)				X			

109

110

111 2.2.1 Grab sampling of the wastewater and sludge

112 Grab samples from wastewater were collected from each sampling site in water process. Three
113 replicates ($n = 3$) were taken from each sample types consecutively. Sampling was done by
114 pumping water from the wastewater stream was (at depth ~ 1 m) onto the designated filter with an
115 electric pump (Biltema art.17-953). Filtering set up previously designed for microplastic sampling
116 in wastewaters was used (Talvitie *et al.* 2015). The respective filter mesh sizes were 300, 100 and
117 $20 \mu\text{m}$, giving size fractions of $> 300 \mu\text{m}$, $100 - 300 \mu\text{m}$ and $20 - 100 \mu\text{m}$ (SD fig S2). The volume
118 of each sample (Table 2.) was measured with a flow meter (Gardena Water Smart Flow Meter)
119 attached to the pump. This volume of filtered water depended on the water quality and filter size.
120 The volumes of replicate samples differed, since the water quality varied.

121 This sampling method is not applicable for influent water due to its high amount of organic material
122 which rapidly clogs the filters allowing only small water volumes to pass. For the influent sampling
123 a metallic beaker to collect water from the wastewater stream surface was used and the samples
124 were later filtered in laboratory with the same filter set up.

125 Samples from the excess sludge and reject water were collected with the same method as influent
126 samples, while dried sludge was collected by hands from the conveyor belt after dewatering
127 process. All sludge and reject water samples were placed into pre-cleaned plastic containers and
128 transported into the laboratory for filtering. The sludge and reject water samples were diluted before
129 filtering by mixing subsamples of wet sludge (1 gram), reject water (10 gram) and dry sludge (0,2
130 gram) with 1 liter of tap water. Diluted sludge and reject water samples were then filtered with the
131 filtering device as the wastewater samples. Details of different samples are presented in table 2. To
132 prevent contamination during the sampling, all equipment was rinsed carefully with tap water prior
133 to sampling.

134

135 Table 2. The sample volumes/weights with sampling locations and mesh sizes of the filters

Sampling sites	sample volume/weight	sample volume/weight	sample volume/weight
	300 μm filter	100 μm filter	20 μm filter
Influent	0.1 l	0.1 l	0.1 l
After pre-treatment	50 – 333 l	7 – 10 l	0.5 l
after AS	200 – 333 l	20 – 30 l	1 l
Effluent	1000 l	100 l	2 l
Excess sludge	1.2 ml = 1 g	1.2 ml = 1 g	1.2 ml = 1 g
Dry sludge	0.2 g	0.2 g	0.2 g
Reject water	10 ml = 10 g	10 ml = 10 g	10 ml = 10 g

136

137 **2.2.2 Composite sampling**

138 24-hour composite samples were collected from all sites in water process (Table 3.). Composite
139 samplers (ISCO 3700) in each sampling location took flow proportional, discrete samples at regular
140 15 min. intervals over 24-hour period of time. The samples were collected into plastic containers
141 placed in refrigerators. Both, the containers and refrigerators were carefully cleaned prior to
142 sampling to avoid contamination from room dust. From the containers, samples were poured into
143 the filter device using a measuring glass. Sampling was performed three times during the week;
144 Tuesday, Thursday and Sunday (Table 1.). To assess possible contamination, blank samples of tap
145 water were used as controls following the same methodological procedure as the actual samples.

146

147

148

149 Table 3. The 24-hour composite sample volumes with sampling locations and mesh sizes of the
150 filter.

Sampling site	sample volume with 300 μm filter	sample volume with 100 μm filter	sample volume with 20 μm filter
Influent	0.1 l	0.1 l	0.1 l
After pre-treatment	13.2 – 14.5 l	8.5 – 10.5 l	0.5 l
After AS	11 – 14.5 l	11 – 14.5 l	1 l
Effluent	10.5 – 13.5 l	10.5 – 13.5 l	2 l
Control	14.5 l	14.5 l	2 l

151

152 **2.2.3 Sequential sampling**

153 Influent and effluent sampling were performed simultaneously with automated samplers (ISCO
154 3700). The samplers took 24 samples at 1-hour interval. After sampling, 3 samples (3 hours) were
155 pooled together, resulting 8 samples per sampling. To avoid contamination, the bottles and the
156 samplers were cleaned carefully before the sampling. The sampler device formed a closed system
157 for entire sampling period. After the sampling, bottles were immediately closed until filtering.
158 Control samples prepared of tap water were preserved in pre-cleaned bottles in the sampler for 24-
159 hours and treated the same way as the actual sequential samples.

160 **2.3 Analyses of microlitter**

161 **2.3.1 Analyses with stereo microscope**

162 All the filtered samples were stored in clean Petri dishes. Samples were visually examined using a
163 stereomicroscope (Fiberoptic-Heim LQ 1100, magnification $\times 50$), light projected from above to get
164 good image of surface structure of microlitter particles. The particles were counted, divided into

165 fibers, fragments, flakes, films and spheres and their coloration documented. The morphological
166 properties of the particles were inspected with micro tweezers to exclude soft, easily disintegrating
167 organic materials. Organic litter like food scraps and paper (cellulose), were excluded from the
168 examination. To detect possible contamination during transport and microscopic analyses, three
169 control samples were carried along during the sampling in the WWTP.

170 **2.3.2 Material identification of microlitter**

171 The chemical composition of microlitter particles from effluent samples were analysed with
172 imaging Fourier Transform infrared spectrometer (FTIRi) (Spectrum Spotlight 300, PerkinElmer,
173 Waltham, MA, USA). All together three effluent samples, one replica from each day (Monday,
174 Wednesday and Saturday) were chosen for analyses and all together 752 particles were included
175 into the analyses. Particles were hand-sorted from the filters with fine tip tweezers under the
176 stereomicroscope and carefully rinsed with distilled water to remove organic matter that was
177 attached to them. Rinsed particles were placed onto ZnSe windows designed for FTIRi microscopy
178 and let to dry for few hours. Each sample window was photographed with the FTIRi and particles
179 identified from the picture. The particles were exposed one by one to infrared radiation in wave
180 length region of $700 - 4000 \text{ cm}^{-1}$ using single point transmission mode. To analyse the spectra
181 obtained with FTIRi, the Thermo Scientific™ Hummel Polymer and Additives FT-IR Spectral
182 Library was used. The materials of textile fibers were analyzed with textile fiber library made
183 ourselves from pure model fibers (purchased from Lahti University of Applied Sciences, Faculty of
184 Technology) (SD fig. S3 – S10). The model fibers included cotton, wool, linen, silk, viscose,
185 polyester, polyacryl, polyamide, and polypropene fibers.

186

187

188 2.3.3 The data analyses

189 The removal of microlitter during different treatment steps were statistically analyzed using analysis
190 of variance (ANOVA).

191 For the microlitter balance analyses, the average microlitter flow was calculated by multiplying the
192 average microlitter concentrations with the corresponding average flow along each wastewater
193 treatment step. The equation can be expressed as:

$$194 \text{ ML} = \text{Q C}$$

195 ML (microlitter d⁻¹) is the flux of microlitter and Q (L d⁻¹) is wastewater, reject water or sludge
196 flow. C (ML L⁻¹) is the average microlitter concentration measured in the wastewater, reject water
197 or sludge.

198 The retention capacity of microlitter in WWTP was calculated as:

$$199 \frac{([\text{Influent}] - [\text{Effluent}])}{[\text{Influent}]} \times 100$$

200

201 3. Results and Discussion

202 3.1 Grab sampling of wastewater and sludge

203 Most of the microlitter particles (97.4% - 98.4%) were removed already during mechanical and
204 chemical pre-treatment phase (table 4). During pre-treatment, microlitter concentrations decreased
205 significantly in all three sampling occasions (Monday: $F = 190.668 > 7.709$; $P < 0.05$, Wednesday:
206 $F = 14.246 > 7.709$; $P < 0.05$ and Saturday: $F = 37.689 > 7.709$; $P < 0.05$). This finding is consistent
207 with previous studies examining the removal of microlitter during wastewater treatment processes
208 (Talvitie *et al.* 2015, Carr *et al.* 2016, Murphy *et al.* 2016). Pre-treatment in Viikinmäki WWTP
209 includes screening, grit removal and chemically enhanced primary sedimentation. Purpose of the
210 treatment is to remove grit, particulate materials as well as phosphates and colloidal matter from the

211 wastewater. According to our results, these techniques remove efficiently also microlitter. In
212 influent, majority of microlitter particles are probably attached to grit and larger particles and
213 removed from the wastewater along with them.

214 Concentration continued to decrease significantly also during AS process, except on Wednesday
215 when the variation between the replicates were so high that although microlitter was clearly
216 removed to a lower level, the result was insignificant with P-value 0.05 (Monday: $F = 7.966 >$
217 7.709 ; $P < 0.05$, Wednesday: $F = 7.472 > 7.709$; $P < 0.05$, Saturday: $F = 42.097 > 7.709$; $P < 0.05$).
218 Together AS process further decreased the microlitter concentration in range [7% - 20%] (table 4).
219 During the treatment, microlitter particles are mixed with flocs and settled into the sludge during
220 secondary sedimentation. Small part of the microlitter, however, escapes the treatment.

221 According to our results, the tertiary treatment, biologically active filter (BAF), didn't decrease
222 microlitter concentration (table 4). The main purpose of BAF in Viikinmäki WWTP is to remove
223 nitrogen from the wastewater but according to the preliminary study (Talvitie *et al.* 2015) the
224 filtering effect was expected to remove a proportion of the microlitter particles left in the secondary
225 effluent. After the BAF, the discharged effluent contained 0.7 – 3.5 microlitter particle per liter of
226 wastewater. This result differs from the study of Carr *et al.* (2016), where no microlitter after the
227 tertiary treatment was detected. Differences in the sampling methods, especially volumes make this
228 comparison difficult, but both works clearly underline the efficiency of the first steps of the
229 processes in the purification efficiency. The two WWTPs also differ in the techniques used for
230 tertiary treatments, which may have caused differences in the removal result. Where BAF appears
231 to be inefficient to remove microlitter, other techniques, like gravity filters, may have a better
232 removal capacity.

233

234

235 Table 4. The average microlitter concentration, including all the fractions ($> 300 \mu\text{m}$, $100 - 300 \mu\text{m}$
 236 and $20 - 100 \mu\text{m}$), in influent, after pre-treatment, after AS and in effluent. Data is given in number
 237 of microlitter particles per L^{-1} of wastewater. Figures represent mean values $\pm\text{SE}$, $n = 3$.

Sampling site	Monday	Wednesday	Saturday
Influent	636.7 (± 38.8)	686.7 (± 155.0)	380 (± 52.2)
After pre-treatment	14.2 (± 4.0)	10.9 (± 2.9)	9.9 (± 1.0)
After AS	1.0 (± 0.6)	1.3 (± 0.9)	2.0 (± 0.2)
Effluent	3.2 (± 0.7)	0.7 (± 0.6)	3.5 (± 1.3)

238

239 To evaluate the microlitter balance of the WWTP, excess sludge, dry sludge and reject water were
 240 also analyzed for one sampling day. The results are collected to table 5. The average wastewater
 241 flow during the sampling day (Wednesday) was $2.82 \times 10^8 \text{ L d}^{-1}$.

242 Table 5. The average microlitter concentrations and flow rates in excess + raw sludge mixture, dry
 243 sludge and reject water. Data is given in number of microlitter particles per g^{-1} or L^{-1} of sludge.

244 Concentrations are mean values $\pm\text{SE}$, $n=3$ and flows day average.

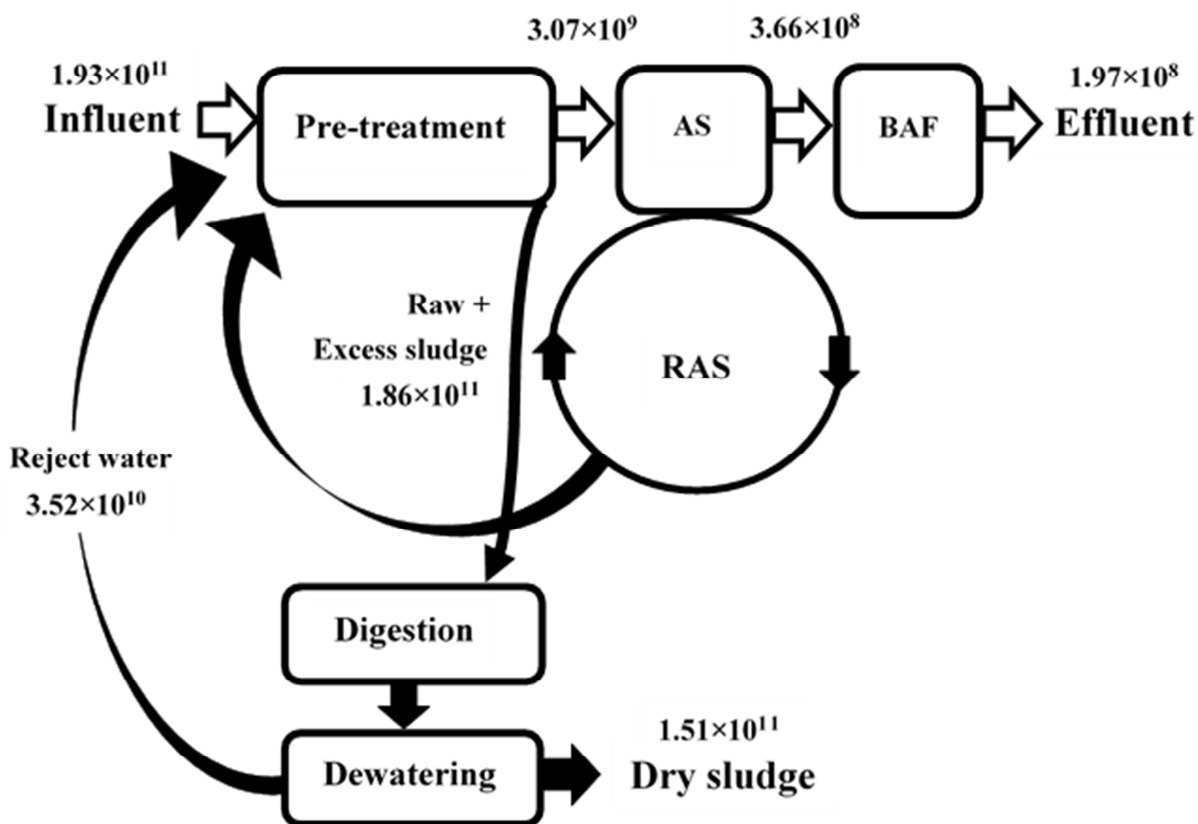
Sampling point	Recess + raw sludge	Dry sludge	Reject water
Microlitter per gram	76.3 (± 4.3)	186.7 (± 26.0)	12.9 (± 0.3)
Microlitter per liter	63611.1 (± 3543.7)	NA	12866.7 (± 275.4)
Average flow (L d^{-1})	2.92×10^6	1.84×10^5	2.74×10^6

245

246 A microlitter balance over the treatment process is presented in Fig. 3. The overall balance and the
 247 balance of the pre-treatment are summing up to an error of approximately 20% of the influent load.

248 This indicates that the microlitter sampling and analysing have been successful in different parts of
 249 the water and solid flows. When not removed from the WWTP with effluent or dried sludge,

250 microlitter particles are recycled inside the WWTP with the activated sludge and reject water.
 251 During the digestion organic matter is degraded, but non-biodegradable or slowly degradable
 252 particles like plastics are not affected by this sludge handling. In dewatering of raw and excess
 253 sludge, the reject water is separated and conducted into the beginning of the wastewater treatment
 254 process. Balance analysis indicates that reject water acts as considerable inner source of microlitter
 255 particles back into the process (fig 1.). Approximately 20% of the microlitter removed from the
 256 process is recycled back in the reject water whereas 80% of the microlitter is contained in the dried
 257 sludge.



258

259 Fig 1. Microlitter balance and distribution in the WWTP. White arrows represents wastewater and
 260 black-coloured represents sludge. Figures are microlitter flow per day (ML/d).

261 The dried sludge is transported to composting fields. After composting, the product is used in green
 262 construction. As Viikinmäki WWTP produces annually around 60,000 tonnes of dried sludge,

263 enormous amounts of microlitter are ending up to the environment with sludge.

264 3.2 24-hour composite samples

265 24-hour composite sampling was performed to study the average concentration and removal of
 266 microlitter during the wastewater treatment over one day period. Sampling was performed three
 267 times during the sampling week; Monday to Tuesday, Wednesday to Thursday and Saturday to
 268 Sunday (Table 6.). The method was also evaluated for possible microlitter monitoring purposes.

269 Table 6. 24-hour composite samples. The microlitter concentrations in influent, after pre-treatment,
 270 after AS and in effluent. Data is given in number of microlitter particles per L⁻¹ of wastewater.

Sampling point	Tuesday	Thursday	Sunday
Influent	900.0	390.0	630.0
After pre-treatment	23.8	10.1	4.1
After AS	2.8	3.1	1.5
Effluent	2.8	1.4	1.4
Blank	0.4	0.8	0,6

271

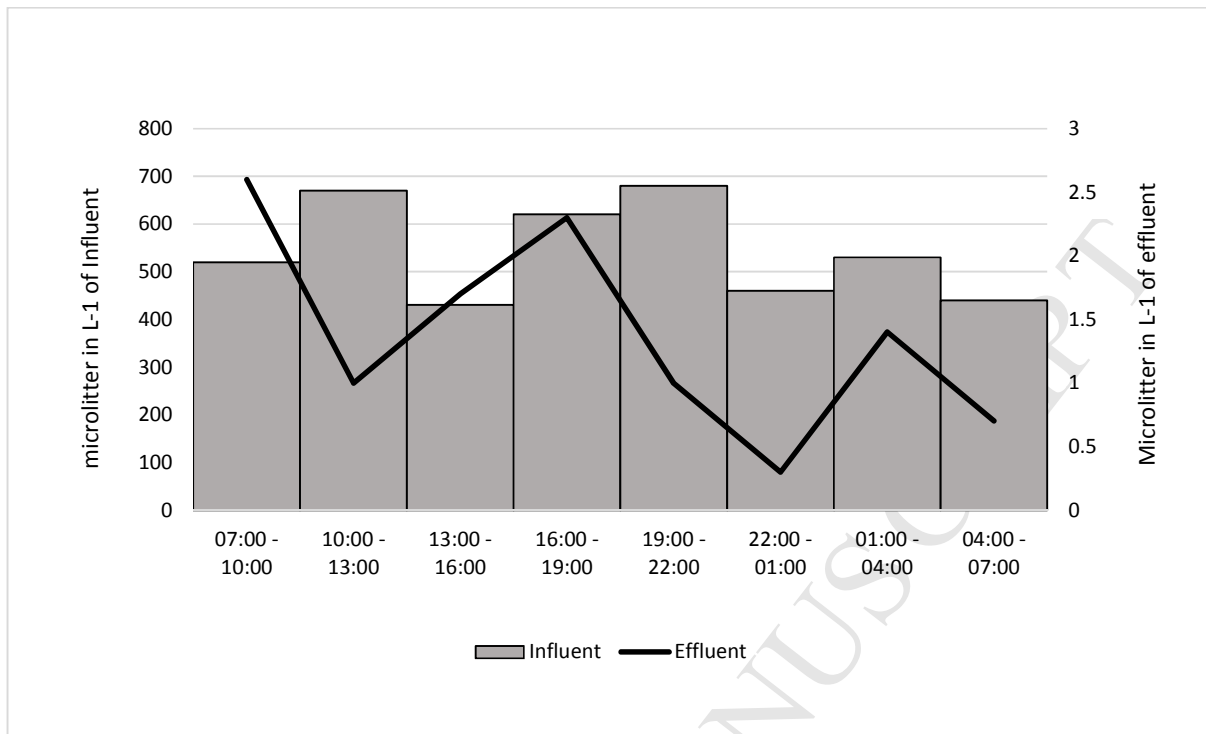
272 The trend of microlitter removal during different treatment steps determined with 24 – hour
 273 composite sampling was very well in line with grab sampling results. Also the microlitter content
 274 per liter was in the same range. Surprisingly the variation between sample days especially in
 275 influent wastewater was larger with 24h composite samples (390.0 – 900.0 particles per L⁻¹) than
 276 with grab samples (380±52.2 – 686.7±155.0).

277 Automated samplers provide an easy microlitter sampling protocol. This can be utilized in
 278 monitoring. However, if the microlitter concentration is very low, composite samples might give
 279 false zero results, as the sample volumes are so small (in our study, only 10-20 liters). In this case,

280 grab sampling with larger sample volumes might be required. Another clear disadvantage of
281 composite sampling is the microlitter contamination. Microlitter type that easily contaminates the
282 samples is textile fiber. As it is also one of the most common microlitter types in wastewater (Habib
283 *et al.* 1996, Zubris *et al.* 2005, Talvitie *et al.* 2015), the contamination distorts the results and easily
284 leads to overestimation of microlitter and microplastics in wastewater. During this study, a great
285 care was taken to minimize contamination during the composite sampling. However, the efforts,
286 contamination of microlitter particles was continuously detected, being between 0.4 – 0.8
287 microlitter per L⁻¹ of water, which accounts for over 30% of the estimated microlitter content in the
288 effluent water. No contamination was detected due to the transportation and analyses.

289 **24-hour sequential sampling**

290 In-day variation in the microlitter concentration was detected in both influent and effluent samples
291 (Fig 2). The night time (10 pm – 7 am) concentrations were generally lower, average concentrations
292 in influent 476.7 and effluent 0.8 microlitter L⁻¹, compared to day time (7 am – 10 pm)
293 concentrations of 584 in influent and 1.7 microlitter per L⁻¹ in effluent. No contamination was
294 detected from blank sequential samples. The lowest microlitter concentration during day time was
295 detected during 1 – 4 pm and microlitter concentration increases towards the early evening hours.
296 This might have had an impact on our results from grab sampling, as the sampling was performed
297 always in day time during low concentration hours.



298

299 Fig 2. 24-hour sequential samples. Microlitter concentrations in influent and effluent. Data is given
 300 in number of microlitter particles per L⁻¹ of wastewater. One sample consist of three-hour period
 301 pooled together.

302 The variation trend in microlitter concentration is in line with day-time activities in households
 303 which influence the amount of microlitter coming to the WWTPs. The in-day variation in
 304 microlitter concentration has to be taken into account when evaluating the total amounts of
 305 microlitter entering and leaving the WWTP with discharged effluents. These results supports the
 306 use of composite sampling or e.g long-term large-scale sampling described by Carr *et al.* (2016)
 307 when evaluating the role of WWTPs as source of microlitter pollution.

308

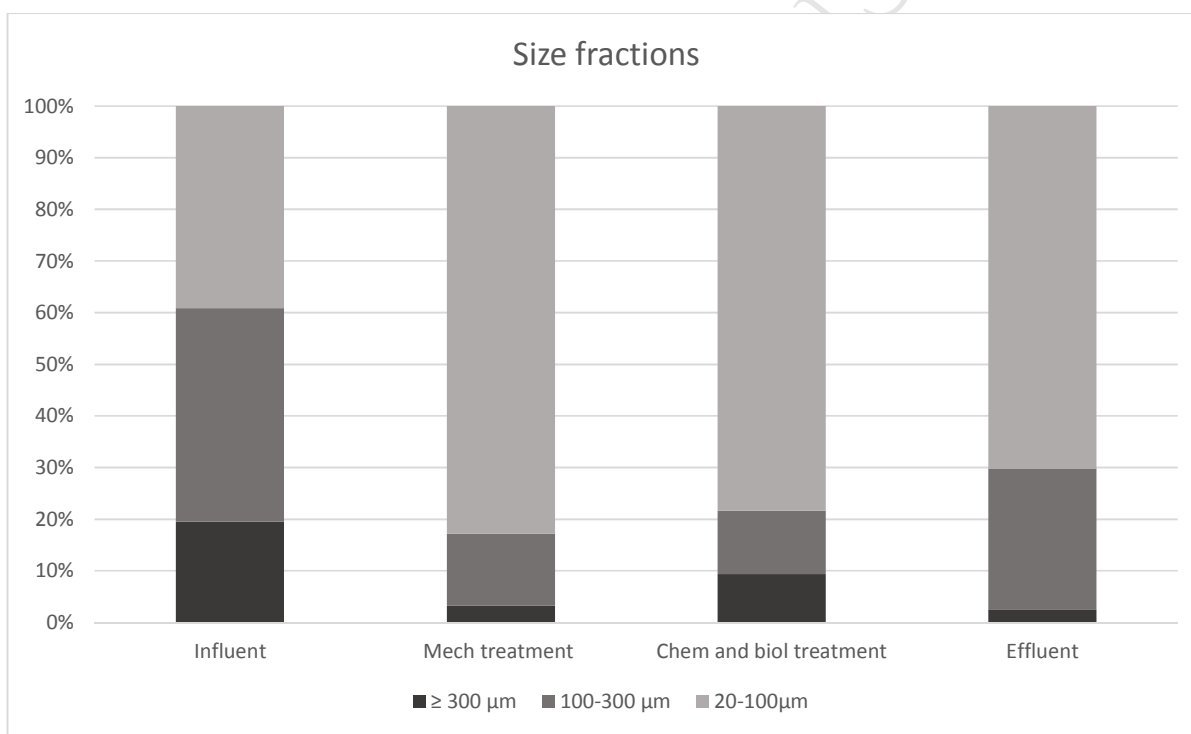
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310

311 3.3 Analyses of microlitter

312 3.3.1 Analyses with stereomicroscope

313 The proportion of the different microlitter size fractions differed between the wastewater treatment
 314 steps (Fig. 3). Pre-treatment had the greatest impact on microlitter size distribution, efficiently
 315 removing larger size fractions (≥ 300 and $100 - 300 \mu\text{m}$), and particles in the smallest fraction ($20 -$
 316 $100\mu\text{m}$) became most abundant. In effluent samples, the slight increase of particles of $100 - 300 \mu\text{m}$
 317 in size was caused by the emergence of clear crystal fragments in this fraction. Origin of these
 318 fragments remained unknown.

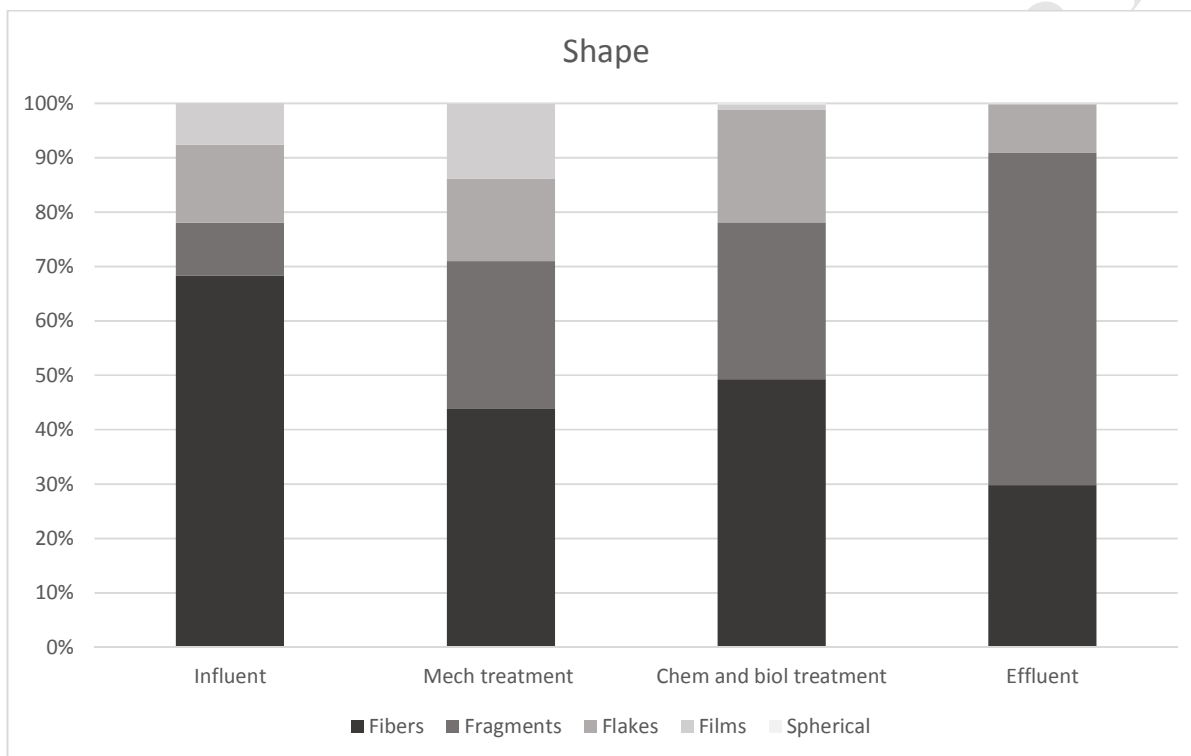


319

320 Figure 3. The proportion of the different size classes of microlitter during the wastewater treatment
 321 steps. The distribution is based on number of particles.

322 Also the proportion of particle types/shapes changed during the purification process (Fig. 4). In the
 323 influent the fibers made up around 70 % of the total microlitter particles, and in effluent only 30 %.
 324 Most of the fibers were removed already during pre-treatment. In influent, textile fibers probably

325 attach easily to grit and to other larger organic waste material and settle down to sludge efficiently
 326 during primary sedimentation. The proportion of fragments increased during the treatment. Majority
 327 of the fragments detected in effluent consisted of clear fragments. Relative proportion of flakes was
 328 approximately the same in all treatment phases.



329

330 Figure 4. The proportion of microlitter shape categories during the wastewater treatment phases.
 331 The distribution is based on number of particles.

332 3.3.2 Material identification

333 All together 752 microlitter particle were included in the material identification. However, the
 334 overall success rate for material identification was relatively low, only 18 % (table 8). Especially
 335 clear fragments remained unrecognized. Reasons for overall weak success rate were unrecognizable
 336 particles (e.g. inorganic minerals and metals), limits of the FTIR spectroscopy and weak quality
 337 infrared spectra. The cause for weak quality spectra can be e.g the biofilm contaminating the
 338 particles. The biofilm in our wastewater samples generally gave spectrum peaks at wavenumber of

339 1000 – 2500 cm^{-1} . In those wavenumbers the biofilm was blocking the possible peaks from the
 340 actual material of the particle and hindered the analyses. Scanning electron microscopy with energy
 341 dispersive spectrometer (SEM-EDS) could probably increase the percentages for successful
 342 analyses by e.g. confirming inorganic composition of the particles. Some chemical treatments have
 343 been tested for removal of biological matter from samples when analysing the microplastics from
 344 wastewater (Tagg *et al.* 2015). However, if natural materials e.g cotton textile fibers are included
 345 into the examination, the chemical treatments can harm the materials and complicate the analyses.

346 Table 8. Microlitter types from effluent samples included into the material analyses, the success rate
 347 of the analyses and detected materials (PE=polyethylene, PS=polystyrene, PP= polypropylene
 348 PES=polyester, NA = not available).

Particle types	Included	Successfully analyzed	%	Materials
Fibers	108	108	100	See fig.7
Fragments				
Blue	26	3	12	PE x 2, PS
Black	18	3	17	PE x 2, PP
Red	4	1	25	PP
Yellow	3	3	100	PES
Green	6	0	0	NA
Brown	1	0	0	NA
White	4	1	25	PP
Clear	507	14	2,8	PE (minerals?)
Silver	2	0	0	NA (metals?)
All	571	25	4	
Flakes				

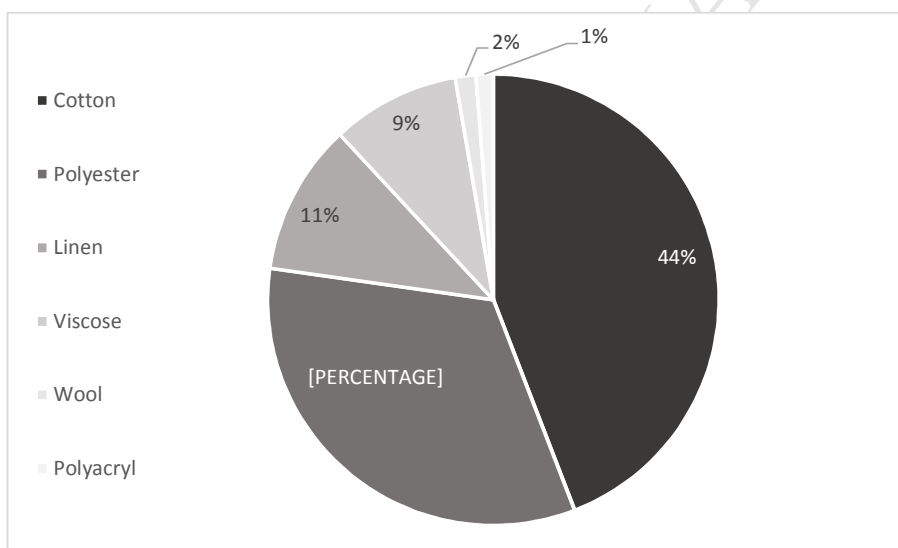
Blue	3	0	0	NA
Black	4	0	0	NA
Red	2	0	0	NA
Clear	1	0	0	NA
Silver	55	0	0	NA (metals?)
All	65	0	0	
Films				
Black	1	0	0	NA
Yellow	1	0	0	NA
Clear	3	1	33	PP
All	5	1	20	
Spherical				
Black	1	0	0	NA
Yellow	1	0	0	NA
White	1	0	0	NA
All	3	0	0	

349

350 All of the 108 fibers from effluent samples were successfully analysed with FTIRi. Textile fiber is
 351 easily identifiable litter type and this helps further material analyses. However, majority of the
 352 natural textile fibers gave relatively weak spectrums and it was hard to found a match for them in
 353 commercial polymer libraries. To solve this problem, the spectrums were analysed with textile fiber
 354 library made from model fibers. With the help of the library, materials of all textile fibers were
 355 ascertained.

356 The top two textile fibers were cotton (44%) and polyester (33%) (Fig 5.). In overall, 66% of the all
 357 textile fibers were natural fibers of cotton, linen or wool. Natural textile fibers have been more or

358 less excluded from the scientific microlitter studies and the focus has been more on synthetic fibers.
 359 This is probably due the general perception that because natural fibers degrade faster and are
 360 “organic” by nature, they do not pose harm to the environment. Opposite opinions state that natural
 361 fibers may actually act as carriers to harmful substances because textiles from organic fibres have
 362 often been treated with harmful chemicals, such as flame retardants, Also, like microplastics,
 363 natural fibers may also absorb pollutants from surrounding water and faster degradation compared
 364 to synthetic ones can lead to quicker release of chemicals into the surrounding environment
 365 (Ladewig *et al.* 2015). As the textile fiber, from washing of clothes (Browne *et al.* 2011), is one of
 366 the most common litter types in wastewater and both the natural and synthetic fibers can have
 367 negative impacts in environment, we recommend that when evaluating the role of WWTPs as point
 368 source of microlitter, natural textile fibers would be included into the examination.



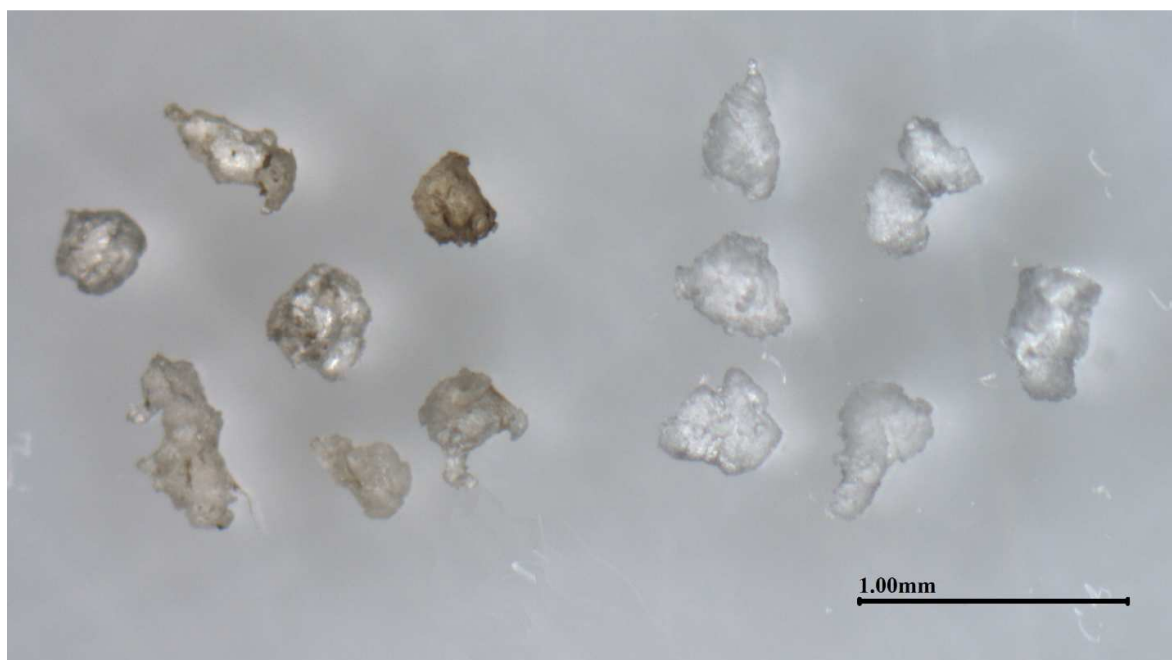
369

370 Figure 5. Materials of fibers and their percentage in effluent samples.

371 Microlitter type observed frequently in our effluent samples was clear polyethylene fragment, the
 372 type found in some widely used cleansing scrubs (fig 6, SD fig S11). When a particle has a very
 373 distinct and recognizable profile (size, shape and color), it is possible to find its origin. For example

374 Carr *et al.* (2016) discovered that the most common particle found in their effluent samples, blue
375 polyethylene fragments, resembled the ones found in toothpaste.

376



377

378 Figure 6. On the left: polyethylene fragments, covered with brownish biofilm, from effluent
379 samples. On the right: polyethylene fragments from cleansing scrubs.

380 However, clear PE fragments consisted only a small part from all clear particles found from our
381 effluent samples (Table 8). Most of the clear particles were hard crystals which remained
382 uncharacterized. Wastewater contains a lot of microlitter and microplastic particles that are
383 unrecognizable and it is difficult to estimate their possible material before material analyses.

384 Particles are either secondary microparticles deriving from fragmentation of larger litter items or
385 primary microparticles from unknown source. Analyzing these particles is particularly challenging
386 when material is not suitable for FTIR spectroscopy and hence the spectra gained from the analyses
387 are unclear.

388

389

390 3.4.3 The role of WWTPs as an entrance route for microlitter

391 The amount of microlitter entering the marine environment with the effluent varied between
 392 2.0×10^8 to 7.9×10^8 particles per day and the ascertained average MP load varied between 1.7×10^6 to
 393 1.4×10^8 particles per day (Table 9).

394 Table 9. Flow rates (m^3/d), microlitter concentrations (ML/m^3) and microlitter load (ML/d),
 395 microplastic concentrations (MP/m^3) and microplastic load (MP/h) from WWTP with effluent.

Date	Monday 14.9	Wednesday 16.9	Saturday 19.9
Flow rate (m^3/d)	219024	281750	224294
ML concentration (ML/m^3)	3200	700	3500
ML outflow (ML/d)	$\sim 7.0 \times 10^8$	$\sim 2.0 \times 10^8$	$\sim 7.9 \times 10^8$
MP concentration (MP/m^3)	651	6	161
MP outflow (MP/d)	$\sim 1.4 \times 10^8$	$\sim 1.7 \times 10^6$	$\sim 2.0 \times 10^7$

396

397 In their study Murphy *et al.* 2016 estimated the daily discharge of 6.5×10^7 MPs in large secondary
 398 WWTP (PE 650 000, treating 260 954 m^3 of wastewater per day) and Carr *et al.* (2016) calculated a
 399 daily discharge of 0.93×10^6 MPs also in large (treating 1.06 million m^3 of wastewater per day)
 400 secondary WWTP. Our results, together with these studies, indicate that secondary and even tertiary
 401 WWTPs may constitute a considerable source of microlitter and microplastics given the large
 402 volumes of effluent discharged to the aquatic environment constantly.

403

404 4. Conclusions

405 Our work provides a detailed information on the stepwise removal of microlitter in a tertiary level
 406 WWTP. Most of (97%) the microlitter in wastewater was removed during the pre-treatment and AS

407 treatment further decreased (7% - 20%) the microlitter concentration. Tertiary treatment BAF didn't
408 have any significant impact on microlitter concentration. Pre-treatment had the greatest effect also
409 on microlitter size distribution, efficiently removing larger size classes of ≥ 300 and $100 - 300 \mu\text{m}$.
410 Of the different types of microlitter, fibers and films were most efficiently removed from the
411 wastewater. The microlitter balance confirmed the applicability of our sampling and analysing
412 methods and showed that 0.1% of the microlitter entering the plant ended up in the effluent and the
413 rest was removed with the sludge. 20% of the microlitter in the removed sludge returned to the
414 process with reject water.

415 Automated composite samplers can provide relatively easy microlitter sampling protocol. With grab
416 sampling, larger sample volumes and hence statistically more representative results are gained. The
417 method is neither so sensitive to contamination. However, the grab sampling method requires much
418 more time and effort compared to composite sampling with automated equipment. The grab
419 sampling also ignores the in-day variations in microlitter concentration. If microlitter is examined
420 over longer period or regularly e.g. for monitoring purposes composite sampling with automated
421 samplers can offer a practical sampling tool.

422 According to our results 2.0×10^8 to 7.9×10^8 microlitter per day and 1.7×10^6 to 1.4×10^8 microplastics
423 per day was discharged into the Baltic Sea with effluent. Given the large volumes of effluent
424 discharged to the aquatic environment constantly, even tertiary level WWTPs may constitute a
425 considerable source of microlitter and microplastics.

426

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433

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Highlights

- The microlitter retention capacity in investigated WWTP was over 99%.
- The size and shape of microlitter particles has impact on their removal in WWTP.
- Microlitter balance analysis for the wastewater treatment process for performed.
- Microlitter sampling protocol for monitoring purposes was investigated.
- WWTPs can constitute entrance route for microlitter into the aquatic environment.